

## TURBULENT PRANDTL NUMBER IN A CHANNEL FLOW FOR $Pr = 0.025$ and $0.71$

**Hiroyuki Abe**

Japan Aerospace Exploration Agency  
Chofu, Tokyo 182-8522, Japan  
habe@chofu.jaxa.jp

**Robert Anthony Antonia**

Discipline of Mechanical Engineering  
University of Newcastle  
NSW 2308, Australia  
robert.antonio@newcastle.edu.au

### ABSTRACT

DNS databases in a turbulent channel flow with passive scalar transport and a constant time-averaged heat-flux boundary condition have been used to examine the variation of the turbulent Prandtl number ( $Pr_t$ ) across the channel. Two values of the molecular Prandtl number  $Pr$  are considered (0.025 and 0.71); in each case, data were obtained for four values of  $h^+$  (180, 395, 640, 1020). For  $Pr=0.71$ ,  $Pr_t$  is 1.1 at the wall, varies between 0.9 and 1.1 in the region  $y^+ < 100$ , and is represented by  $0.9 - 0.3(y/h)^2$  for  $y/h > 0.2$ . The closeness to unity near the wall is attributed to the excellent similarity between the velocity and scalar fields, whereas the decrease in magnitude in the outer region is most likely associated with the unmixedness of the scalar. A similar description for  $Pr_t$  is not possible for  $Pr=0.025$  due to the strong conductive effects. In this case, the near-wall limiting value is unlikely to approach unity.

### INTRODUCTION

The turbulent Prandtl number, which is defined as the ratio of the turbulent eddy viscosity ( $\nu_t$ ) to the turbulent eddy diffusivity ( $a_t$ ),

$$Pr_t = \frac{\nu_t}{a_t} = \frac{\overline{uv} \frac{d\overline{\Theta}}{dy}}{\overline{v\theta} \frac{d\overline{U}}{dy}} \quad (1)$$

is an important quantity in the context of computing (e.g. via RANS and LES) turbulent shear flows with scalar transport ( $u$ ,  $v$ ,  $w$  denote the streamwise, wall-normal and spanwise velocity fluctuations, respectively, and  $\theta$  is the temperature fluctuation. Upper case quantities represent instantaneous values;  $x$ ,  $y$ ,  $z$  are the streamwise, wall-normal and spanwise directions, respectively. An overbar denotes the averaged value with respect to space and time). However, its accurate measurement is difficult especially in the near-wall region (e.g. Launder 1976). Firm conclusions have hence not been formulated with respect to the detailed dependence of  $Pr_t$  on the Reynolds and Prandtl numbers and also the distance from the wall. Its value is sometimes assumed to be constant (viz.  $Pr_t=0.9$ ). The closeness to unity implies a close similarity between the velocity and scalar fields. However, this similarity may break down when  $Pr \ll 1$  or  $Pr \gg 1$  (e.g. Reynolds 1975).

Direct numerical simulations (DNSs) have yielded accurate near-wall turbulence quantities, thus allowing significant improvement in near-wall turbulence models (e.g. Mansour et al. 1988). Antonia and Kim (1991) examined the near-wall behavior of  $Pr_t$  in a turbulent channel flow using the DNS database obtained from Kim and Moin (1988). Three values of  $Pr$  (0.1, 0.71 and 2) were examined at  $h^+ \equiv u_\tau h / \nu = 180$  ( $u_\tau$ ,  $h$ ,  $\nu$  denote the friction velocity, channel half-width and kinematic viscosity, respectively. A superscript + denotes normalization by wall units.). The near-wall limiting value was 1.1, almost independently of  $Pr$ . For other DNSs at low/moderate Reynolds numbers ( $h^+ \leq 395$ ) (Kasagi and Ohtsubo 1993; Kawamura et al. 1999), the same wall limiting value was also reported for moderate but not very low values of  $Pr$  (e.g.  $Pr=0.025$ ). However, it is not clear what happens at larger  $h^+$  (i.e.  $h^+ > 395$ ) and to what extent  $Pr_t$  varies throughout the channel. These issues need to be sorted out before further progress in turbulence scalar modelling can be made.

In the present study, we examine the behavior of  $Pr_t$  across the channel along with that of turbulent heat fluxes using the DNS databases by Abe et al. (2004, 2009). Four values of  $h^+$  (180, 395, 640 and 1020) are investigated for two types of working fluid, namely mercury ( $Pr=0.025$ ) and air ( $Pr=0.71$ ). The main objective is to quantify this behavior and clarify the functional dependence of  $Pr_t$  with respect to  $h^+$ ,  $Pr$ , and  $y$ . Attention is also given to turbulence modelling for  $a_t$  (e.g. Nagano and Kim 1988; Yoshizawa 1988), where the relationship between  $Pr_t$  and  $R$  (time-scale ratio) is discussed.

### DNS DATABASES

The present databases have been obtained from DNSs in a turbulent channel flow with passive scalar transport for  $h^+ = 180, 395, 640$  and  $1020$  at  $Pr=0.025$  and  $0.71$  by Abe et al. (2004, 2009). The thermal boundary condition employed is a constant time-averaged heat-flux (Kasagi et al. 1992; Kasagi and Ohtsubo 1993). The numerical methodology is briefly as follows. A fractional step method is used with semi-implicit time advancement. The Crank-Nicolson method is used for the viscous terms in the  $y$  direction and

Table 1 Domain size, grid points and spatial resolution.

$h^+$		180	395	640	1020
$L_x \times L_y \times L_z$		12.8h × 2h × 6.4h			
$L_x^+ \times L_y^+ \times L_z^+$		2304 × 360 × 1152	5056 × 790 × 2528	8192 × 1280 × 4096	13056 × 2040 × 6528
$Pr=0.71$	$N_x \times N_y \times N_z$	768 × 128 × 384	1536 × 192 × 768	2048 × 256 × 1024	2048 × 448 × 1536
	$\Delta x^+, \Delta y^+, \Delta z^+$	3.00, 0.20 ~ 5.93, 3.00	3.29, 0.15 ~ 6.52, 3.29	4.00, 0.15 ~ 8.02, 4.00	6.38, 0.15 ~ 7.32, 4.25
$Pr=0.025$	$N_x \times N_y \times N_z$	256 × 128 × 256	512 × 192 × 512	1024 × 256 × 1024	2048 × 448 × 1536
	$\Delta x^+, \Delta y^+, \Delta z^+$	9.00, 0.20 ~ 5.93, 4.50	9.88, 0.15 ~ 6.52, 4.94	8.00, 0.15 ~ 8.02, 4.00	6.38, 0.15 ~ 7.32, 4.25

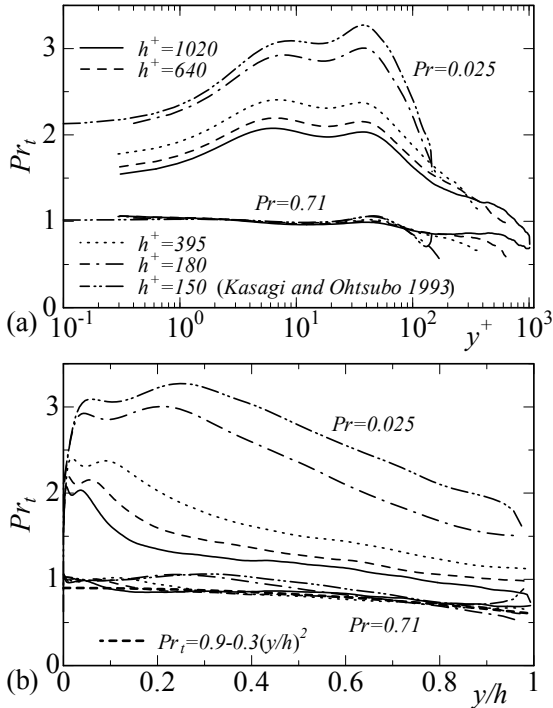


Figure 1: Distributions of  $Pr_t$ : (a) inner scaling; (b) outer scaling.

the 3rd-order Runge-Kutta method for the other terms. Three exceptions are the cases for  $h^+ = 180, 395$  and  $640$  at  $Pr=0.025$ , where the 2nd-order Adams-Bashforth method is employed instead of the 3rd-order Runge-Kutta method. For the spatial discretization, a 4th-order finite difference central scheme is used in the  $x$  and  $z$  directions, with a 2nd-order central scheme in the  $y$  direction. Further details and validation of turbulence statistics can be found in Abe et al. (2004, 2009) and Antonia et al. (2009). The computational domain size ( $L_x \times L_y \times L_z$ ), number of grid points ( $N_x \times N_y \times N_z$ ) and spatial resolution ( $\Delta x, \Delta y, \Delta z$ ) are given in Table 1. Note that for  $h^+=1020$  the same velocity field has been used for computations at  $Pr=0.025$  and  $0.71$ , whereas for  $h^+=180, 395$  and  $640$  different velocity fields have been used for simulations at each  $Pr$ . Also for the latter three  $h^+$  at  $Pr=0.71$ , two scalar fields with different thermal boundary conditions (viz. the constant heat flux (Kasagi et al. 1992) and the internal source heating (Kim and Moin 1989)) have been time-advanced simultaneously with the same velocity field, where attention was given to small scales (Abe et al. 2009) so that the spatial resolution is finer than that for the other cases. A few results with the internal source heating are also included for comparison.

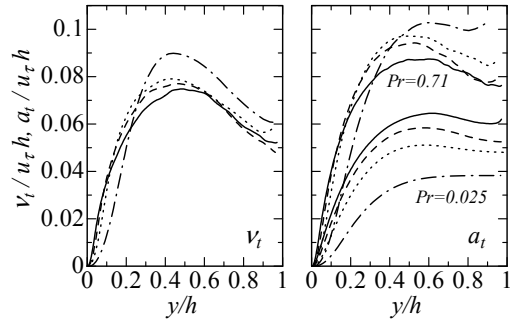


Figure 2: Distributions of  $v_t$  and  $a_t$  normalized by outer variables.

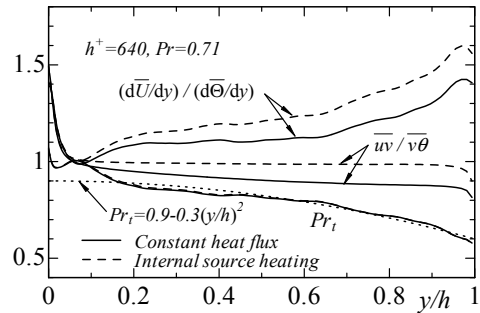


Figure 3: A comparison of  $Pr_t$  between the constant heat flux and internal source heating ( $h^+=640$  and  $Pr=0.71$ ).

## RESULTS AND DISCUSSION

Distributions of  $Pr_t$ , normalized by inner and outer variables, are shown in Fig. 1. For  $Pr=0.71$ , the inner and outer scalings are valid for  $y^+ < 100$  and  $y/h > 0.2$ , respectively. The wall limiting value is 1.1, independently of  $h^+$ , consistent with the finding of Antonia and Kim (1991) at  $h^+=180$ . For  $y^+ < 100$ ,  $Pr_t$  does not vary significantly; it remains in the range 0.9 to 1.1. In particular, the magnitude is large near the wall, which is attributed to the close analogy between the velocity and scalar fields (Antonia et al. 2009; Abe and Antonia 2009) (see also Fig. 4). The magnitude of  $Pr_t$  however decreases gradually towards the channel centerline (see a difference between  $v_t$  and  $a_t$  in Fig. 2). In the outer region ( $y/h > 0.2$ ), the distributions are described approximately by

$$Pr_t = 0.9 - 0.3(y/h)^2, \quad (2)$$

which is similar to the suggestion by Rotta (1964). Eq. (2) is also applicable when the heating is done with an internal source (see the almost perfect correspondence between the constant heat flux and the internal source heating in Fig. 3). Further, other DNS data (Kim and Moin 1988; Kawamura et al. 1998) indicate that Eq. (2) seems to apply not only for air but also for water (viz.  $Pr = 5 \sim 7$ ).

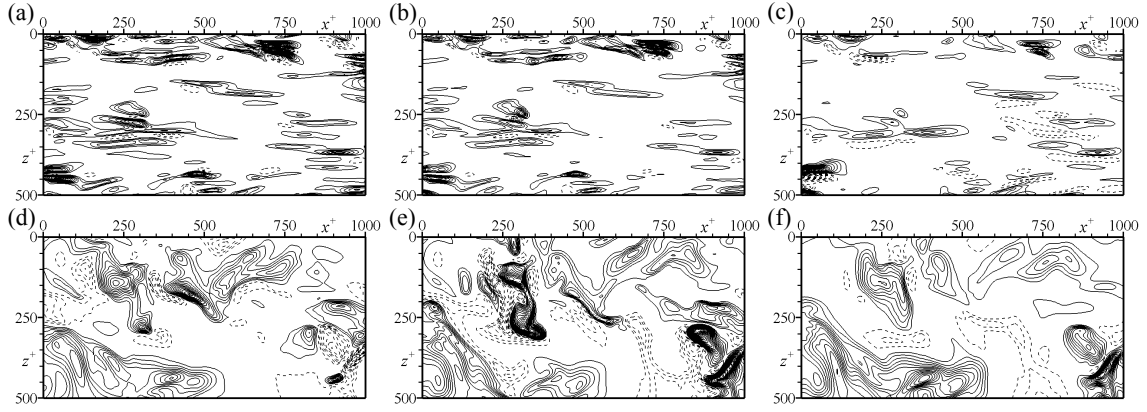


Figure 4: Contours of  $uv$  and  $v\theta$  at  $h^+=1020$ : (a),(d)  $uv$ ; (b),(e)  $v\theta$  for  $Pr=0.71$ ; (c),(f)  $v\theta$  for  $Pr=0.025$ . For (a), (b) and (c),  $y^+=10$  and for (d), (e) and (f),  $y/h=0.4$ . Solid and dashed lines are negative and positive values, respectively. Line increments for  $uv$  and  $v\theta$  for  $Pr=0.71$  are 0.5 independently of  $y$ , whilst those for  $v\theta$  for  $Pr=0.025$  are 0.025 and 0.25 at  $y^+=10$  and  $y/h=0.4$ , respectively.

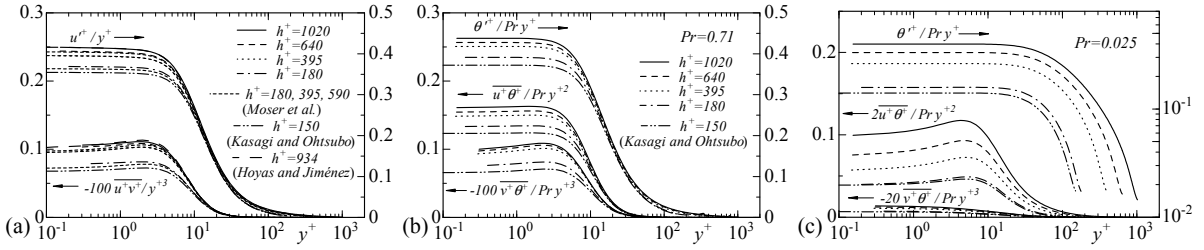


Figure 5: Near-wall limiting behavior for  $u'$ ,  $\theta'$ ,  $\overline{uv}$ ,  $\overline{u\theta}$  and  $\overline{v\theta}$ .

The decrease in magnitude in the outer region is most likely to be associated with the unmixedness of the scalar (Guezennec et al. 1990; Antonia et al. 2009). In this context,  $v\theta$  exhibits sharper interfaces than  $uv$  (see  $x^+=z^+=250$  in Fig. 4), the difference being attributed to the unmixed nature of scalar (distributions of  $\theta$  are not shown here). This leads to a discernible difference in the high wavenumber part of the co-spectra (not shown here), the  $v\theta$  co-spectrum being more energetic than the  $uv$  co-spectrum. Such a difference appears as a small difference between  $\overline{uv}$  and  $\overline{v\theta}$  (note that  $\overline{uv}/\overline{v\theta} < 1$  in Fig. 3), which is related to the difference between  $d\overline{U}/dy$  and  $d\overline{\Theta}/dy$  (see  $(d\overline{U}/dy)/(d\overline{\Theta}/dy) > 1$  in Fig. 3) via the relations for the total shear stress and heat flux. The latter difference can also be discerned in the mean velocity and scalar distributions (not shown here), the gradient of the mean velocity being steeper than that for the mean scalar in the outer region.

For  $Pr=0.025$ , on the other hand, the strong conductive effects affect  $Pr_t$  noticeably. Whilst the magnitude decreases significantly with increasing  $h^+$ , the large departure from unity persists throughout the channel, implying a breakdown of the analogy between the velocity and scalar fields (see a large difference between  $v_t$  and  $a_t$  in Fig. 2). Two local peaks appear at  $y^+=5$  and 45. This is attributed to the difference between the mean velocity and scalar distributions. With regard to Fig. 4, although there is a relatively good similarity in  $v\theta$  between  $Pr=0.025$  and 0.71 in the outer region (the correlation coefficient between Figs. 4e and f is 0.81), the similarity is reduced near the wall (the correlation coefficient between Figs. 4b and c is 0.59). This is because near-wall thermal streaks are not noticeable for

$Pr=0.025$ . Instead, large-scale  $\theta$  structures tend to stretch across both inner and outer regions (Kasagi and Ohtsubo 1993; Abe et al. 2004). Since the latter structures tend to be correlated with  $v$ , the near-wall correlation between  $\theta$  and  $v$  is smaller for  $Pr=0.025$  than  $Pr=0.71$ . Consistently, the magnitude of  $\overline{v\theta}$  is smaller for  $Pr=0.025$  than  $Pr=0.71$  (see Figs. 5b and c). This would explain the near-wall departure of  $Pr_t$  from unity for  $Pr=0.025$ .

The difference in  $Pr_t$  between  $Pr=0.025$  and 0.71 is examined further by investigating its near-wall limiting behavior. Taylor series expansions of  $\overline{U}_1$ ,  $\overline{\Theta}$ ,  $\overline{uv}$ ,  $\overline{v\theta}$  together with  $u'$ ,  $\theta'$  and  $\overline{u\theta}$  are expressed as follows:

$$\overline{U}_1^+ = y^+ - \frac{y^{+2}}{2h^+} + O(y^{+4}), \quad (3)$$

$$\overline{\Theta}^+ = Pr \left( y^+ - \frac{y^{+2}}{2h^+} \right) + O(y^{+4}), \quad (4)$$

$$u'^+ = b_1' y^+ + c_1' y^{+2} + d_1' y^{+3} + O(y^{+4}), \quad (5)$$

$$\theta'^+ = b_\theta' y^+ + d_\theta' y^{+3} + O(y^{+4}), \quad (6)$$

$$\overline{u^+v^+} = \overline{b_1 c_2} y^{+3} + O(y^{+4}), \quad (7)$$

$$\overline{u^+\theta^+} = \overline{b_1 b_\theta} y^{+2} + \overline{c_1 b_\theta} y^{+3} + O(y^{+4}), \quad (8)$$

$$\overline{v^+\theta^+} = \overline{c_2 b_\theta} y^{+3} + O(y^{+4}), \quad (9)$$

where a prime denotes a rms value. With the use of Eqs. (3), (4), (7), (9),  $Pr_t$  may be written as

$$Pr_t = \frac{\overline{b_1 c_2}}{c_2 b_\theta} Pr + O(y^+). \quad (10)$$

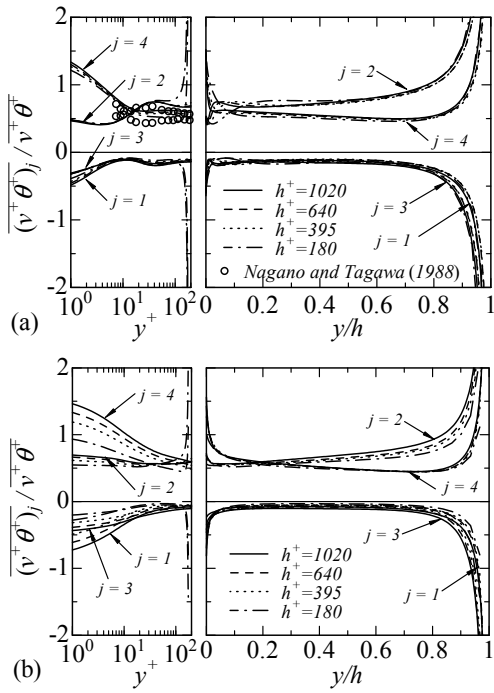


Figure 6: Quadrant analysis for  $\overline{v\theta}$  : (a)  $Pr=0.71$ ; (b)  $Pr=0.025$ .

Eq. (10) implies that the near-wall limiting value of  $Pr_t$  is determined by the relationship between  $\overline{uv}$  and  $\overline{v\theta}$ . The distributions of  $\overline{u^+v^+}/y^{+3}$  and  $\overline{v^+\theta^+}/Pr y^{+3}$  together with  $u^+/y^+$  and  $\theta^+/Pr y^+$  are shown in Fig. 5, which highlights the leading order coefficients of the Taylor series expansions. Also included are the data of  $\overline{u^+\theta^+}/Pr y^{+2}$ . For  $Pr=0.71$ , the near-wall distributions of  $u'$  and  $\overline{uv}$  are similar in shape to those of  $\theta'$  and  $\overline{v\theta}$ , respectively, which is consistent with  $Pr_t = 1.1$  independently of  $h^+$ . The rate of increase in the coefficients from  $h^+=180$  to 395 is significant due to the low  $h^+$  effects (Antonia and Kim 1994), whilst that from  $h^+=395$  to 1020 is moderate (i.e.  $b_\theta'/Pr=0.39, 0.42, 0.43, 0.44$  at  $h^+=180, 395, 640, 1020$ , respectively). For  $Pr=0.025$ , on the other hand, the distributions of  $\theta'$  and  $\overline{v\theta}$  look quite different from those of  $u'$  and  $\overline{uv}$ , respectively, which is consistent with the large departure from unity of  $Pr_t$ . The magnitudes of the coefficients (viz.  $b_\theta', b_1b_\theta, c_2b_\theta$ ) increase logarithmically with increasing  $h^+$  (i.e.  $b_\theta'/Pr=0.16, 0.26, 0.33, 0.40$  at  $h^+=180, 395, 640, 1020$ , respectively). Antonia and Kim (1991) noted that the leading order coefficients for  $\theta'$ ,  $\overline{u\theta}$  and  $\overline{v\theta}$  tend to scale on  $Pr$  when  $Pr \geq 0.1$ . The same trend was also reported by Kawamura et al. (1998). However, this relationship is not applicable for  $Pr=0.025$  (see Figs. 5b and 5c) due to the strong conductive effects. This result has important implications for turbulence modelling. Current models do not reflect the scaling on  $Pr$  (e.g. Nagano and Shimada 1996) correctly.

The above observations imply that there is a significant difference in the generation mechanism for turbulent heat fluxes between  $Pr=0.025$  and  $Pr=0.71$ . To clarify this issue,

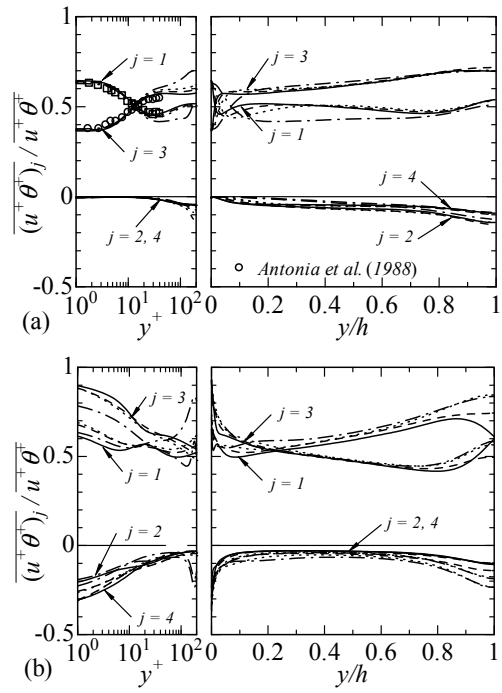


Figure 7: Quadrant analysis for  $\overline{u\theta}$  : (a)  $Pr=0.71$ ; (b)  $Pr=0.025$ . Line patterns are the same as in Fig. 6.

quadrant analysis has been applied to  $\overline{v\theta}$  (Fig. 6). The latter method is often used to examine the generation mechanisms for the turbulent shear stress (Wallace et al. 1972; Willmarth and Lu 1972) and turbulent heat fluxes (Perry and Hoffmann 1976; Antonia et al. 1988). For  $Pr=0.71$ , the contributions from quadrants 2 and 4 are altered in the near-wall region ( $y^+ \approx 17$ ) and are almost similar to those for  $\overline{uv}$  (not shown here). This implies a close similarity in the generation mechanism between  $\overline{uv}$  and  $\overline{v\theta}$  (see also Fig. 4). The distributions are normalized by inner and outer variables in the regions  $y^+ < 100$  and  $y/h > 0.2$ , respectively, as in the case of  $Pr_t$ . In contrast, when  $Pr=0.025$ , the contributions from quadrants 2 and 4 are changed in the outer region ( $y/h > 0.2$ ). Also a significant  $h^+$  effect appears across the channel, consistent with the noticeable dependence of  $\overline{v\theta}$  on  $h^+$  (this is not shown here). A difference in generation mechanism between  $Pr=0.025$  and 0.71 is hence likely in the region  $y/h < 0.2$ .

The same  $Pr$  dependence is observed for  $\overline{u\theta}$  (see Fig. 7), where the scaling range is nearly the same as for  $\overline{v\theta}$  (see Figs. 6 and 7). For  $Pr=0.71$ , the contributions are indeed from quadrants 1 and 3 near the wall, implying a close similarity between  $u$  and  $\theta$  (see also Abe and Antonia 2009). For  $Pr=0.025$ , on the other hand, the contributions from quadrants 2 and 4 cannot be dismissed near the wall, suggesting a breakdown of the analogy between  $u$  and  $\theta$ . It hence follows that in the region  $y/h < 0.2$  turbulent heat fluxes for  $Pr=0.025$  are generated in a different manner than for  $Pr=0.71$ .

The previous considerations imply that, as  $h^+$  increases, the near-wall value of  $Pr_t$  for  $Pr=0.025$ , is unlikely to approach that which corresponds to  $Pr=0.71$ . It is however likely that it may reach it in the outer region. This latter

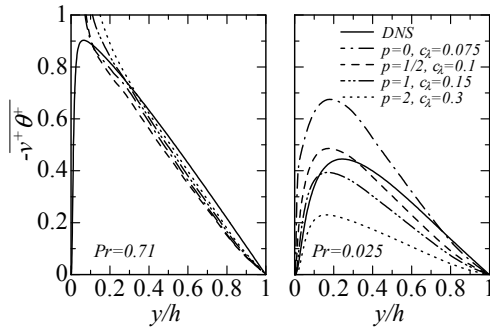


Figure 8: Evaluation of Eq. (14) at  $h^+ = 1020$ .

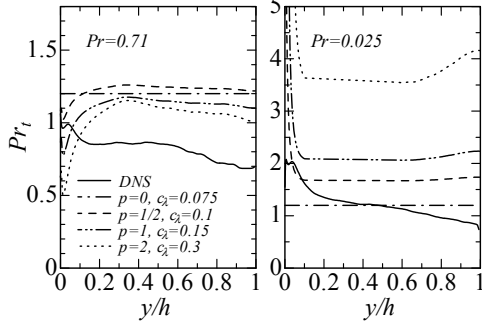


Figure 9: Evaluation of Eq. (17) at  $h^+ = 1020$ .

expectation appears to be supported by the experimental evidence in turbulent pipe flows which indicates that, in the logarithmic region, the magnitude of  $Pr_t$  is nearly the same for  $Pr=0.025$  and  $Pr=0.71$  (see Table 1 of Kader and Yaglom 1972).

Finally, attention is given to turbulence models for  $a_t$  (Nagano and Kim 1998; Yoshizawa 1998). The standard  $v_t$  and  $a_t$  models may be written as

$$v_t = c_\mu f_\mu \frac{k^2}{\varepsilon}, \quad (11)$$

$$a_t = c_\lambda f_\lambda \frac{k^2}{\varepsilon} R^p, \quad (12)$$

where

$$R = \frac{k_\theta / \varepsilon_\theta}{k / \varepsilon} \quad (13)$$

( $k$ ,  $\varepsilon$ ,  $k_\theta$ ,  $\varepsilon_\theta$  and  $R$  denote the turbulent kinetic energy, the mean energy dissipation rate, the temperature variance and the mean scalar dissipation rate and the time scale ratio, respectively) (see also Horitiu 1992). Nagano and Kim (1988) used  $p=1/2$ , whilst Yoshizawa (1988) used  $p=2$ . Note that  $p=0$  corresponds to  $Pr_t = \text{constant}$ . In the present flow, Eq. (12) can also be expressed as

$$-\overline{v\theta} = c_\lambda f_\lambda \frac{k^2}{\varepsilon} R^p \frac{d\overline{\theta}}{dy} \quad (14)$$

Eq. (14) is tested against the DNS data for  $h^+ = 1020$  in Fig. 8, in order to ascertain the optimal value of  $p$ . Note that  $f_\lambda = 1$  and different values of  $c_\lambda$  are used for different  $p$ 's to minimize differences between predictions for  $Pr=0.71$  and the DNS distribution. In Eq. (14), the prediction with  $p=1/2$  (Nagano and Kim 1988) is closest to the DNS data for both Prandtl numbers. The same trend has been also found for other  $h^+$  (the distributions are not shown here). For  $p=1/2$ , Eq. (12) may readily be rewritten as

$$a_t = c_\lambda f_\lambda k \tau_m \quad (15)$$

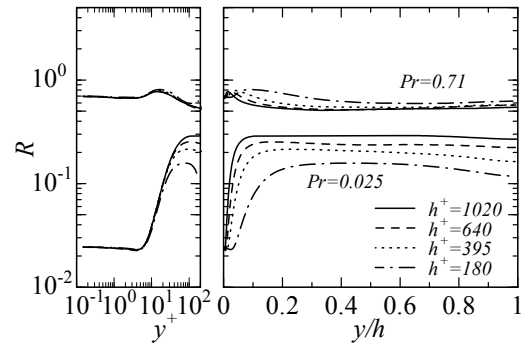


Figure 10: Distributions of  $R$ .

where

$$\tau_m = \left( \frac{k}{\varepsilon} \cdot \frac{k_\theta}{\varepsilon_\theta} \right)^{1/2}, \quad (16)$$

i.e. the velocity and scalar time scales appear via their geometric mean. The present results indicate that Eq. (12) shows promise when predicting the mean scalar distribution for very low  $Pr$  fluid. Nonetheless, there is a discernible deviation from the DNS data even when  $p=1/2$ . Using the  $a_t$  model,  $Pr_t$ , or the ratio of Eqs. (11) and (12),

$$Pr_t = \frac{c_\mu f_\mu}{c_\lambda f_\lambda} R^{-p} \quad (17)$$

(see also Antonia et al. 2009) deviates significantly from the DNS distribution (Fig. 9), where  $f_\mu = 1$  and  $c_\mu = 0.09$  are used. The relationship between  $Pr_t$  and  $R$ , as given by Eq. (17), does not hold in the outer region. This is because, unlike  $Pr_t$ ,  $R$  is approximately constant for both  $Pr=0.025$  and  $0.71$  (see Figs. 1 and 10). It seems likely that the use of a model function and/or the incorporation of a new time scale (e.g. Nagano and Shimada 1996) should reduce the deviation between the model and the DNS data. It should also be noted that for  $Pr=0.025$ ,  $R$ , like  $Pr_t$ , is likely to approach the value corresponding to  $Pr=0.71$  (viz.  $R=0.5$ ) in the outer region.

## CONCLUSIONS

The behaviour in a turbulent channel flow of  $Pr_t$  and the turbulent heat-fluxes has been examined using DNS databases for  $h^+ = 180, 395, 640$  and  $1020$  at  $Pr=0.025$  and  $0.71$  with a constant time-averaged wall heat flux condition (Abe et al. 2004, 2009). The main conclusions are

(1) For  $Pr=0.71$ ,  $Pr_t$  is described in a piecewise manner, viz. i) it is 1.1 at the wall, ii) it varies between 0.9 and 1.1 in the region  $y^+ < 100$ , and iii) it can be approximated by  $0.9 - 0.3(y/h)^2$  for  $y/h > 0.2$ . This description also applies when the heating is via an internal source. Eq. (2) is likely to apply to water as well as air. The closeness of  $Pr_t$  to unity near the wall is attributed to the close similarity between the velocity and scalar fields, whereas the decrease in magnitude in the outer region is most likely to be associated with the unmixedness of the scalar.

(2) For  $Pr=0.025$ ,  $Pr_t$  cannot be described in the same way as for  $Pr=0.71$  due to the strong conductive effects. There is a persistently large departure from unity of  $Pr_t$

throughout the channel, as well as a noticeable dependence on  $h^+$ . Near the wall,  $\theta$  is more poorly correlated with  $v$  than for  $Pr=0.71$ , which is consistent with the departure from unity of  $Pr_t$ . In this context, the near-wall limiting behaviour has shown that contrary to  $Pr=0.71$ , the coefficients  $b_\theta'$ ,  $b_\theta b_\theta$ ,  $c_2 b_\theta$  for  $Pr=0.025$  do not scale on  $Pr$ . This should be taken into account when developing turbulence models.

(3) The quadrant analysis indicates that  $\overline{u\theta}$  and  $\overline{v\theta}$  are generated in different manners in the region  $y/h < 0.2$  between  $Pr=0.025$  and  $Pr=0.71$ . This implies that, as  $h^+$  increases, the magnitude of  $Pr_t$  for  $Pr=0.025$  is not likely to approach that for  $Pr=0.71$  in the near-wall region, although it is likely to attain it in the outer region.

(4) Existing models for  $a_t$  were tested against the DNS data for  $h^+=1020$  for  $Pr=0.025$  and  $0.71$ . The  $p=1/2$  model of Nagano and Kim (1988) provides the closest agreement with the DNS data. However, the relationship between  $Pr_t$  and  $R$  given by Eq. (17) does not hold in the outer region.

#### ACKNOWLEDGEMENTS

Computations performed on Numerical Simulator III at the Computer Centre of the Japan Aerospace Exploration Agency are gratefully acknowledged. We also thank Prof. Kawamura at Tokyo University of Science for his encouragement during the course of this work. HA was partially supported by the Ministry of Education, Culture, Sports, Science and Technology of Japan, Grant-in-Aid for Young Scientists (B), 20760125, 2009. RAA acknowledges the support of the Australian Research Council.

#### REFERENCES

Abe, H., Kawamura, H. and Matsuo, Y., 2004, "Surface heat-flux fluctuations in a turbulent channel flow up to  $Re_\tau = 1020$  with  $Pr=0.025$  and  $0.71$ ," *Int. J. Heat and Fluid Flow* Vol. 25, pp. 404-419.

Abe, H., Antonia, R.A. and Kawamura, H., 2009, "Correlation between small-scale velocity and scalar fluctuations in a turbulent channel flow," *J. Fluid Mech.*, to appear.

Abe, H. and Antonia, R.A., 2009, "Near-wall similarity between velocity and scalar fluctuations in a turbulent channel flow," *Phys. Fluids*, Vol. 21, 025109.

Antonia, R.A. and Kim, J., 1991, "Turbulent Prandtl number in the near-wall region of a turbulent channel flow," *Int. J. Heat Mass Transfer*, Vol. 34(7), pp. 1905-1908.

Antonia, R.A. and Kim, J., 1994, "Low-Reynolds-number effects on near-wall turbulence," *J. Fluid Mech.* Vol. 276, pp. 61-80.

Antonia, R.A., Krishnamoorthy, L. V. and Fulachier, L. 1988, "Correlation between the longitudinal velocity fluctuation and temperature fluctuation in the near-wall region of a turbulent boundary layer," *Int. J. Heat Mass Transfer*, Vol. 31(4), pp. 723-730.

Antonia, R.A., Abe, H. and Kawamura, H., 2009, "Analogy between velocity and scalar fields in a turbulent channel flow," *J. Fluid Mech.*, to appear.

Guezennec, Y., Stretch, D. and Kim, J., "The structure of turbulent channel flow with passive scalar transport," *Proceedings of the 1990 Summer Program of Centre for*

*Turbulence Research* (NASA Ames/Stanford University, Stanford, CA, 1990), pp. 127-138.

Horiuti, K., 1992, "Assessment of two-equation models of turbulent passive-scalar diffusion in channel flow," *J. Fluid Mech.* Vol. 238, pp. 405-433.

Hoyas, S. and Jiménez, J. 2008 "Reynolds number effects on the Reynolds-stress budgets in turbulent channels," *Phys. Fluids*, Vol. 20, 101511.

Kader, B.A. and Yaglom, A.M., 1972, "Heat and mass transfer laws for fully turbulent wall flows," *Int. J. Heat Mass Transfer*, Vol. 15, pp. 2329-2351.

Kasagi, N. Tomita, Y. and Kuroda, A., 1992, "Direct numerical simulation of passive scalar field in a turbulent channel flow," *ASME J. Heat Transfer*, Vol. 114, pp. 598-606.

Kasagi, N. and Ohtsubo, Y., 1993, "Direct numerical simulation of low Prandtl number thermal field in a turbulent channel flow," In: *Turbulent Shear Flows 8* (Edited by Durst et al.), pp. 97-119, Springer, Berlin.

Kawamura, H., Ohsaka, K., Abe, H. and Yamamoto, K., 1998, "DNS of turbulent heat transfer in channel flow with low to medium-high Prandtl number fluid," *Int. J. Heat Fluid Flow*, Vol. 19, pp. 482-491.

Kawamura, H., Abe, H. and Matsuo, Y., 1999, "DNS of turbulent heat transfer in channel flow with respect to Reynolds and Prandtl number effects," *Int. J. Heat Fluid Flow*, Vol. 20, pp. 196-207.

Kim, J. and Moin, P. 1989, "Transport of passive scalars in a turbulent channel flow," In: *Turbulent shear flows 6* (Edited by André et al.), pp. 85-96, Springer, Berlin.

Lauder, B.E., 1976, "Heat and Mass Transport, Topics in Applied Physics," Vol. 12, pp. 231-287.

Mansour, N.N., Kim, J. and Moin, P., 1988, "Reynolds-stress and dissipation-rate budgets in a turbulent channel flow," *J. Fluid Mech.*, Vol. 194, pp. 15-44.

Moser, R.D., Kim, J. and Mansour, N.N., 1999 "Direct numerical simulation of turbulent channel flow up to  $Re_\tau = 590$ ," *Phys. Fluids*, Vol. 11, pp. 943-945.

Nagano, Y. and Kim, C., 1988, "A two-equation model for heat transport in wall turbulent shear flows," *ASME J. Heat Transfer*, Vol. 110, pp. 583-589.

Nagano, Y. and Shimada, M., 1996, "Development of a two-equation heat transfer model based on direct simulations of turbulent flows with different Prandtl numbers," *Phys. Fluids*, Vol. 8, pp. 3379-3402.

Nagano, Y. and Tagawa, M., 1988, "Statistical characteristics of wall turbulence with a passive scalar," *J. Fluid Mech.*, Vol. 196, pp. 157-185.

Perry, E. and Hoffmann, P. H., 1976, "An experimental study of turbulent convective heat transfer from a flat plate," *J. Fluid Mech.* Vol. 77, pp. 355-368.

Reynolds, A.J., 1975, "The prediction of turbulent Prandtl and Schmidt numbers," *Int. J. Heat Mass Transfer*, Vol. 18, pp. 1055-1069.

Rotta, J.C., 1964, "Temperaturverteilungen in der turbulenten grenzschicht an der ebenen platte," *Int. J. Heat Mass Transfer*, Vol. 7, pp. 215-228.

Wallace, J. M., Eckelmann, H. and Brodkey, R. S., 1972, "The wall region in turbulent shear flow," *J. Fluid Mech.* Vol. 54, pp. 39-48.

Willmarth, W. W. and Lu, S. S., 1972, "Structures of the Reynolds stress near the wall," *J. Fluid Mech.* Vol. 55, pp. 65-92.

Yoshizawa, A., 1988, "Statistical modelling of passive-scalar diffusion in turbulent shear flows," *J. Fluid Mech.* Vol. 195, pp. 541-555.